



# **Metropolitan Water Reclamation District of Greater Chicago**

**Welcome to the July Edition  
of the 2024  
M&R Seminar Series**



# NOTES FOR SEMINAR ATTENDEES

- Remote attendees' audio lines have been muted to minimize background noise.  
**For attendees in the auditorium, please silence your phones.**
- A question and answer (Q/A) session will follow the presentation.
- For remote attendees, please use “**Chat**” only to type questions for the presenter. For other issues, please email Pam to SlabyP@mwrdd.org.  
**For attendees in the auditorium, please raise your hand and wait for the microphone to ask a verbal question.**
- The presentation slides will be posted on the MWRD website after the seminar.
- This seminar has been approved by the ISPE for one PDH and approved by the IEPA for one TCH. Certificates will be issued only to participants who attend the entire presentation.

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Wonho Song is a senior engineer at the Los Angeles County Sanitation Districts (LACSD), with over 30 years of technical experience at the LACSD and private consulting companies. Additionally, Wonho serves as an adjunct professor in the Department of Civil and Environmental Engineering at the University of Southern California (USC), where he has been teaching courses on water and wastewater treatment plant design. Wonho holds Bachelor of Science and Master of Science degrees in civil engineering from Korea University, a Master of Science degree in environmental engineering from City University of New York, and a Ph.D. in environmental engineering from USC.



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# A Pilot Study on Biotrickling Filters Using Synthetic Media for Design of Full-Scale Odor Control Facilities

## MWRD Monitoring and Research Seminar

**Warner Song**  
**July 2024**



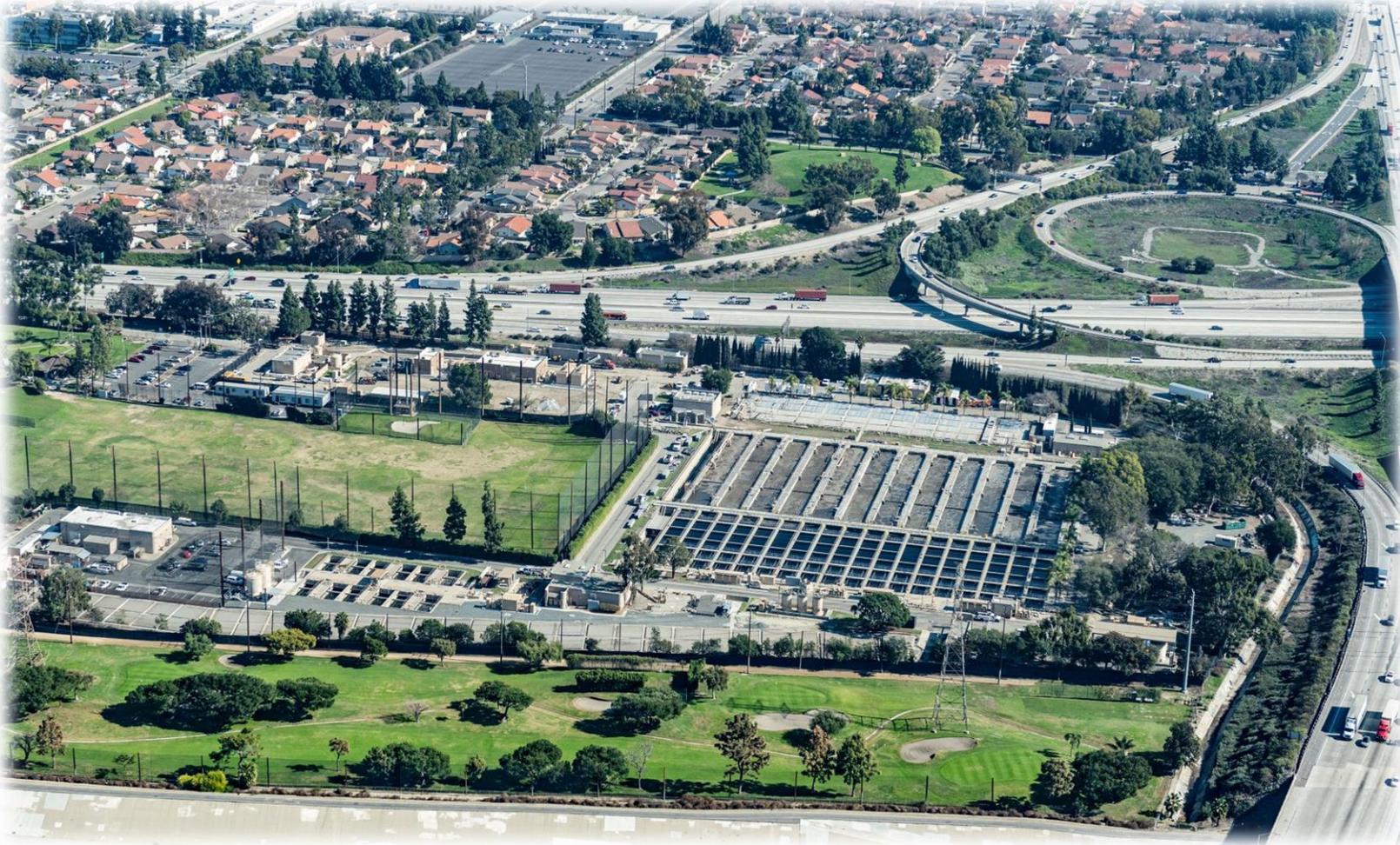
# Los Angeles County Sanitation Districts (LACSD)



- ❑ Wastewater Management:
  - 11 wastewater treatment plants
  - 1,400 miles of sewers
  - Serving ~5.5 million people
  - 850 square miles of service area
- ❑ Solid Waste Management
  - Landfills
  - Recycling centers
- ❑ Converting Waste Into Resources
  - 100 mgd of recycled water
  - 67 megawatts of electricity



# Los Coyotes Water Reclamation Plant (LCWRP)



- ❑ 38 mgd capacity plant
- ❑ Odor complaints from neighbors and nearby commuters
- ❑ Planning is underway for an odor control facility



# Current Odor Control System at LCWRP

- ❑ Activated Sludge Diffusion
  - Collects odorous air, directs it to the suction side of aeration blowers, and diffuses it into aeration tanks
  - Poorly designed ducting layout
  - Corrosive air incompatible with new tech aeration blowers
  
- ❑ Mobile Carbon Scrubbers
  - 8 ft diameter 3 feet deep carbon bed
  - Lasts 3 to 5 days to maintain outlet H<sub>2</sub>S concentration less than 1 ppm



# LACSD's Odor Control Facilities

- ❑ Stand-alone biotrickling filter (BTF)
- ❑ Combined BTF & carbon scrubber
  - BTF removes most  $H_2S$ , and carbon scrubber removes residual  $H_2S$  and other odorous compounds.



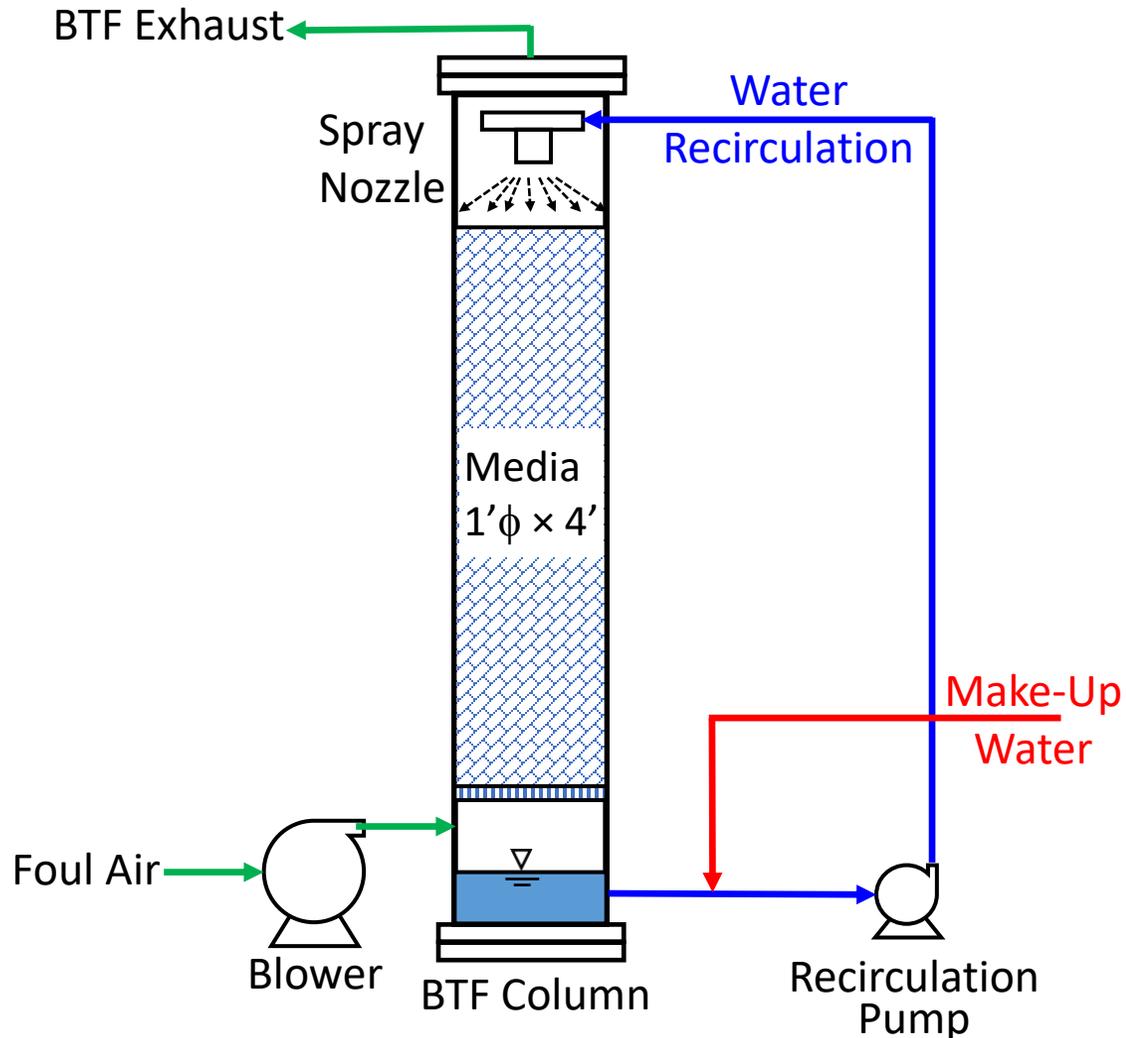
# LACSD's BTF Media



- ❑ Lava rock
  - Performance initially good but declined
  - Heavy (stress on media support)
- ❑ Synthetic media
  - Installed different types at several plants
  - Need side-by-side testing to compare performance → **Pilot testing**



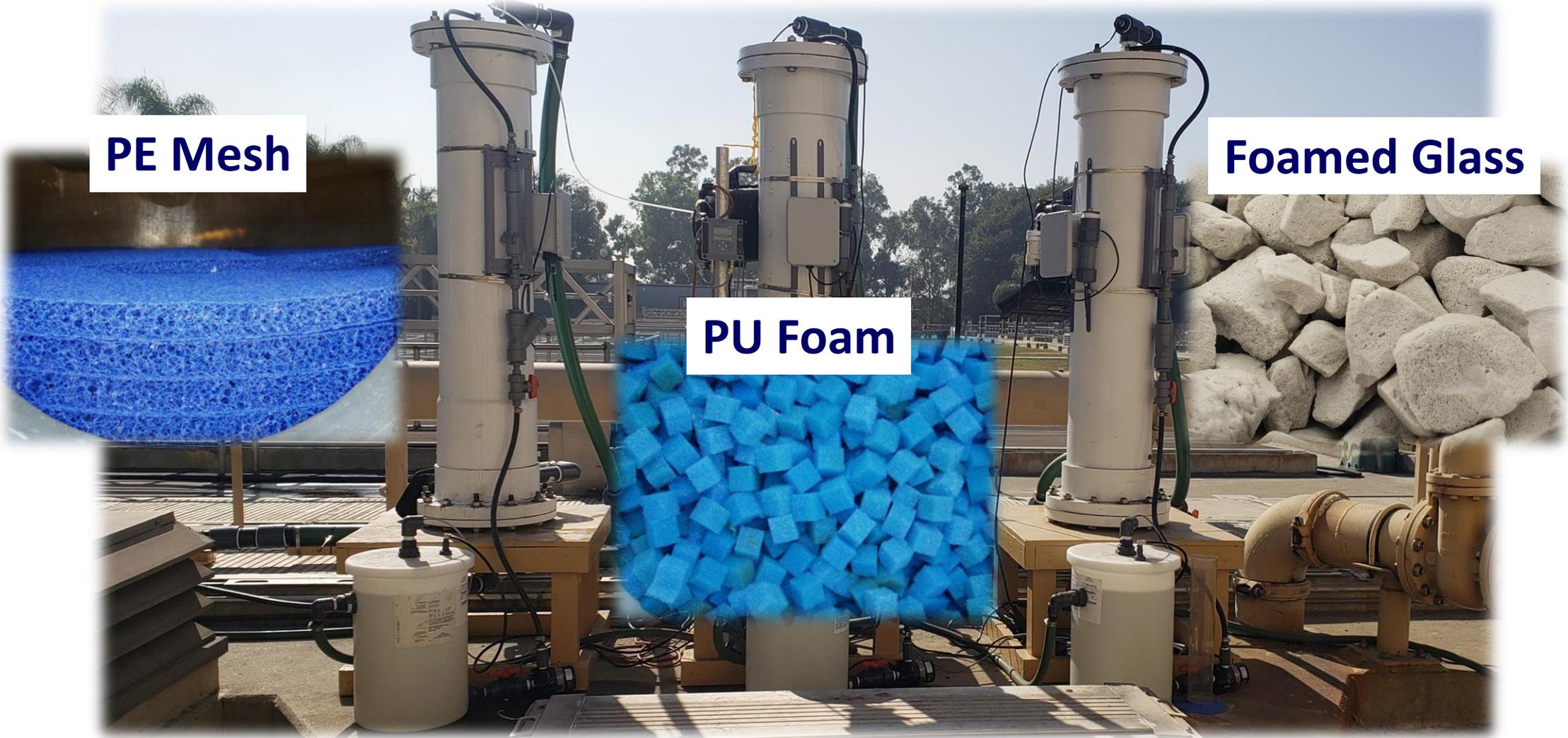
# Schematic of Pilot-Scale BTF



- ❑ Foul Air
  - Upflow
  - $\text{H}_2\text{S}$  is oxidized to  $\text{S}^\circ$  and  $\text{SO}_4$   
→ pH drops
- ❑ Recirculation Water
  - Downflow
  - Provide moisture & nutrients
  - Add make-up water to maintain pH ~2 (1.5–2.5)



# Pilot-Scale BTFs at LCWRP



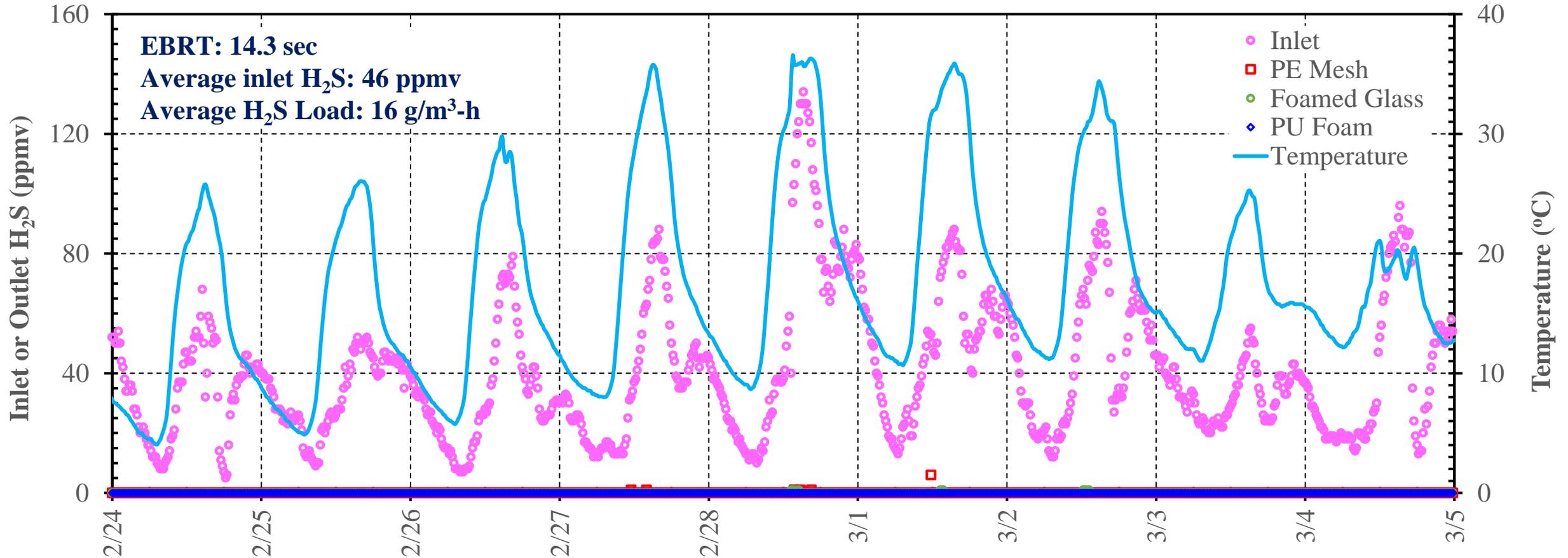
**PE Mesh**

**PU Foam**

**Foamed Glass**



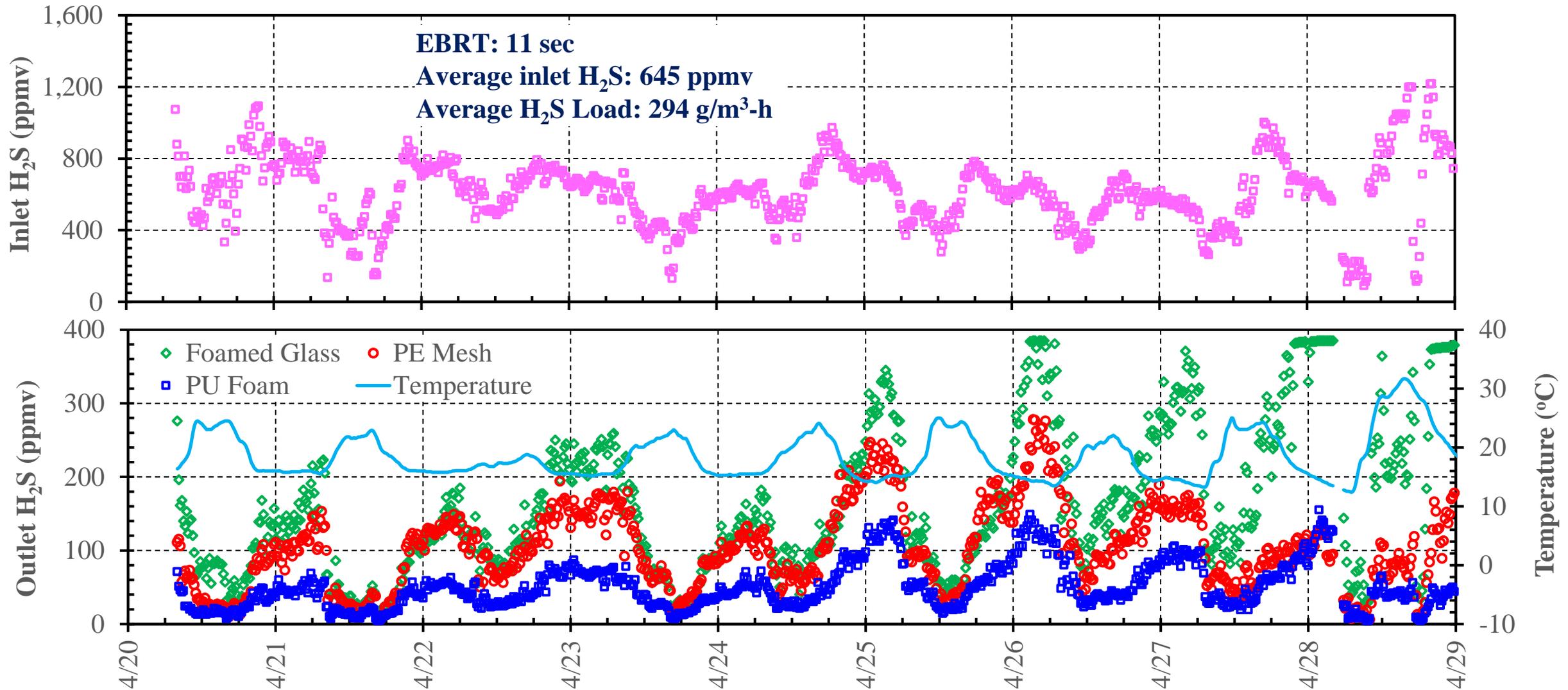
# Diurnal Pattern at Low H<sub>2</sub>S Loading



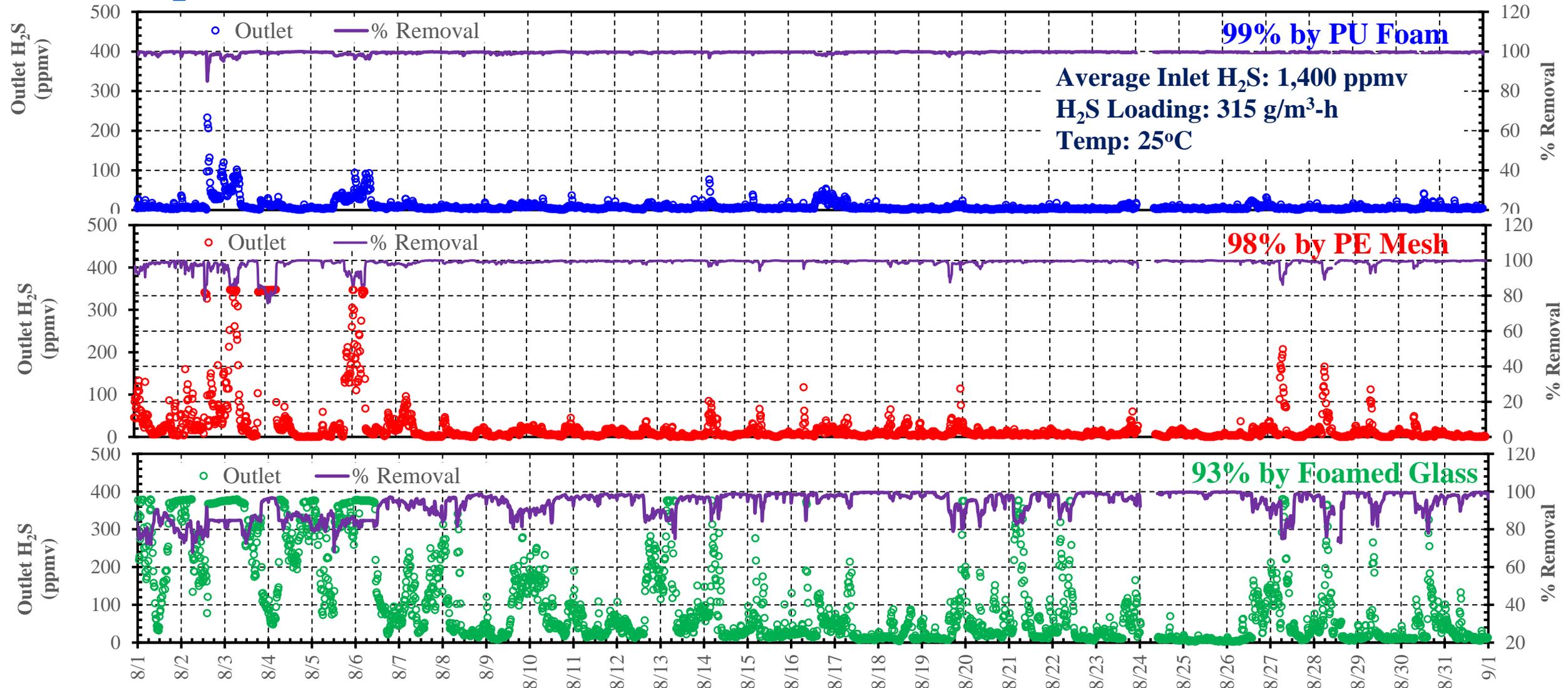
- All media achieve nearly complete H<sub>2</sub>S removal
- Daily peaks in H<sub>2</sub>S load and temperature



# Diurnal Pattern at High H<sub>2</sub>S Loading



# Representative BTF Performance Data



# Synthetic Media Properties

Media	Foamed Glass	PU Foam	PE Mesh (Low Density)	PE Mesh (High Density)
Image				
Material	Calcium Silicate	Polyurethane	Polyethylene	Polyethylene
Specific Surface Area	<b>600 sf/cf</b>	140-160 sf/cf	61 sf/cf	114 sf/cf
Porosity	<b>80-90% (51%)</b>	96-97% ( <b>96%</b> )	92%	94%
Unit Cost	\$10/cf	\$25/cf	\$48/cf	\$50/cf



← Biological growth

← Contact time

- ❑ Poor performance of foamed glass is unexpected
- ❑ Porosity: spec of **80-90%** vs **51%** measured



# Virgin vs Used Foamed Glass



- ❑ Biofilm on external surface only  
→ Internal pores are inaccessible
- ❑ Actual residence time (51% of porosity)  
→ e.g.,  $51\% \times 14 \text{ s of EBRT} = 7.1 \text{ s}$



# Permeability Assessment of Foamed Glass using Dye



After 1 Day



After 1 Week



After 2 Weeks

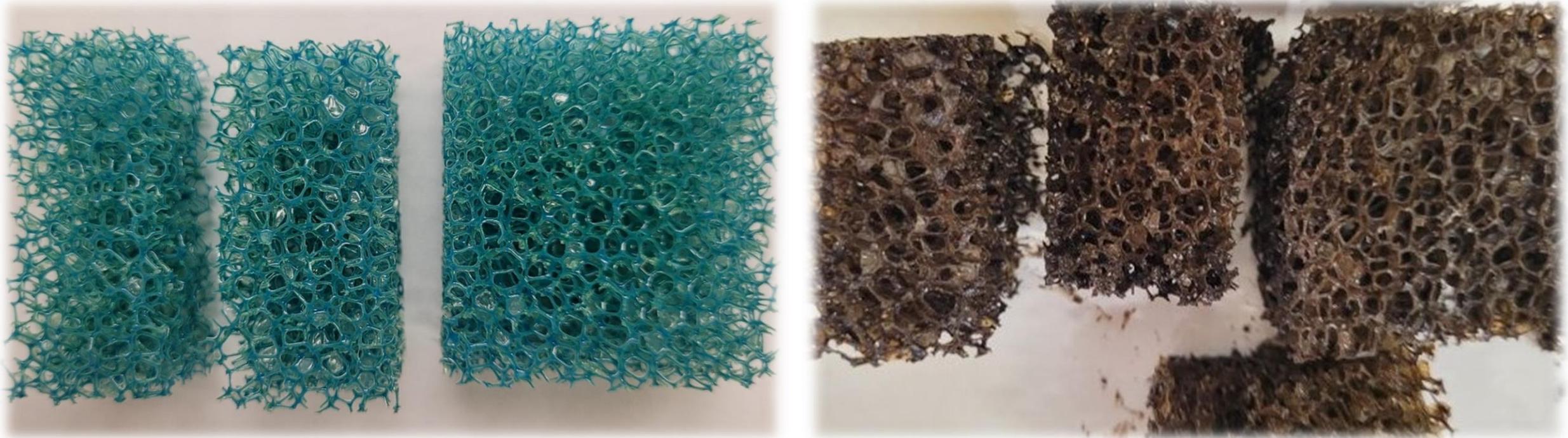


After 4 Weeks

- ❑ Dye gradually penetrated over time but didn't reach internal pores
- ❑ **Internal pores, along with their associated surface area, are inaccessible to water**



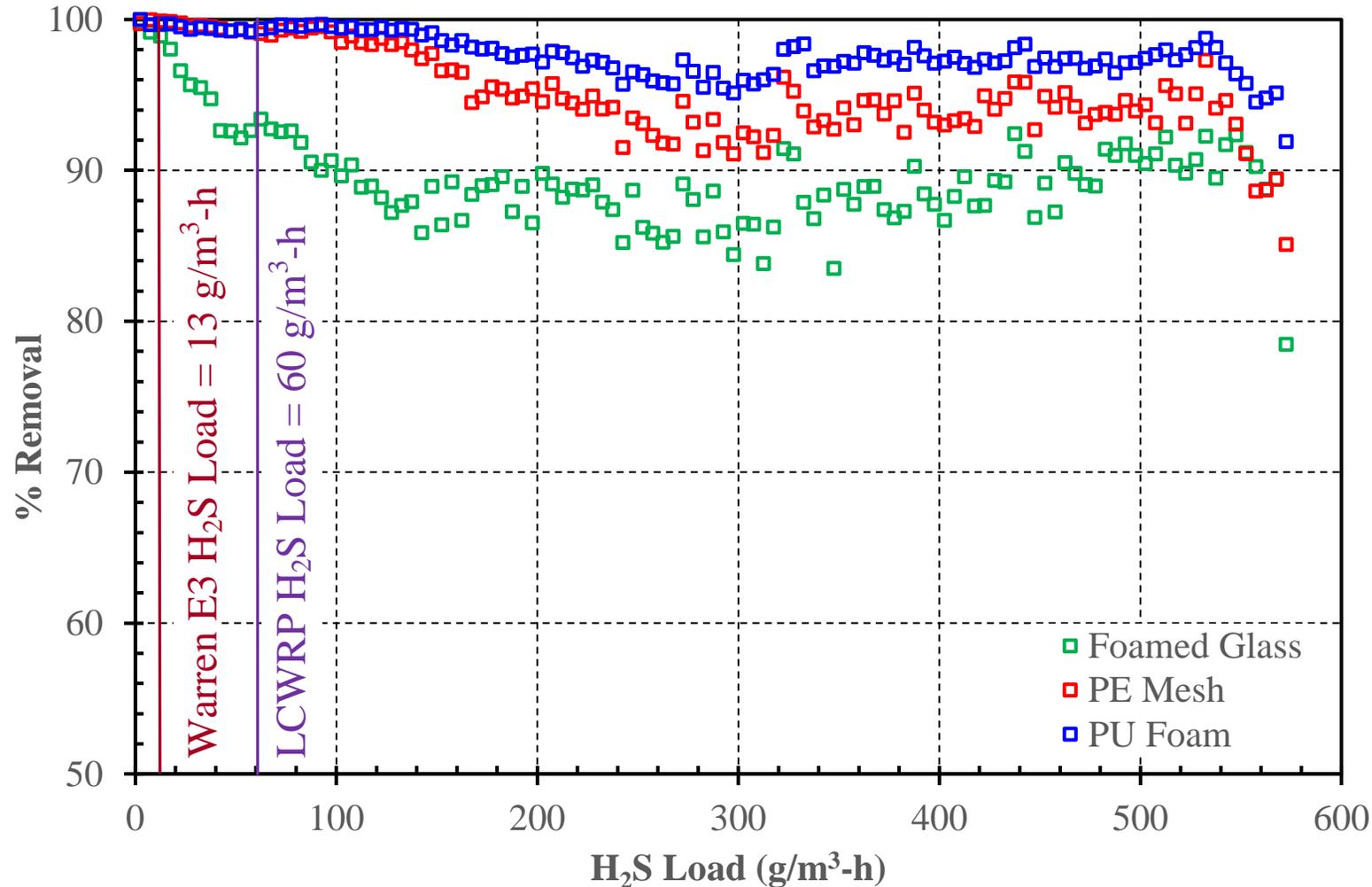
# Cut Faces of Virgin and Used PU Foam



- ❑ Biofilms on both (i) External surface and (ii) Internal pore surface
- ❑ 96% of porosity allows effective residence time close to EBRT  
e.g., Actual residence time =  $96\% \times 14 \text{ s of EBRT} = 13.4 \text{ s}$



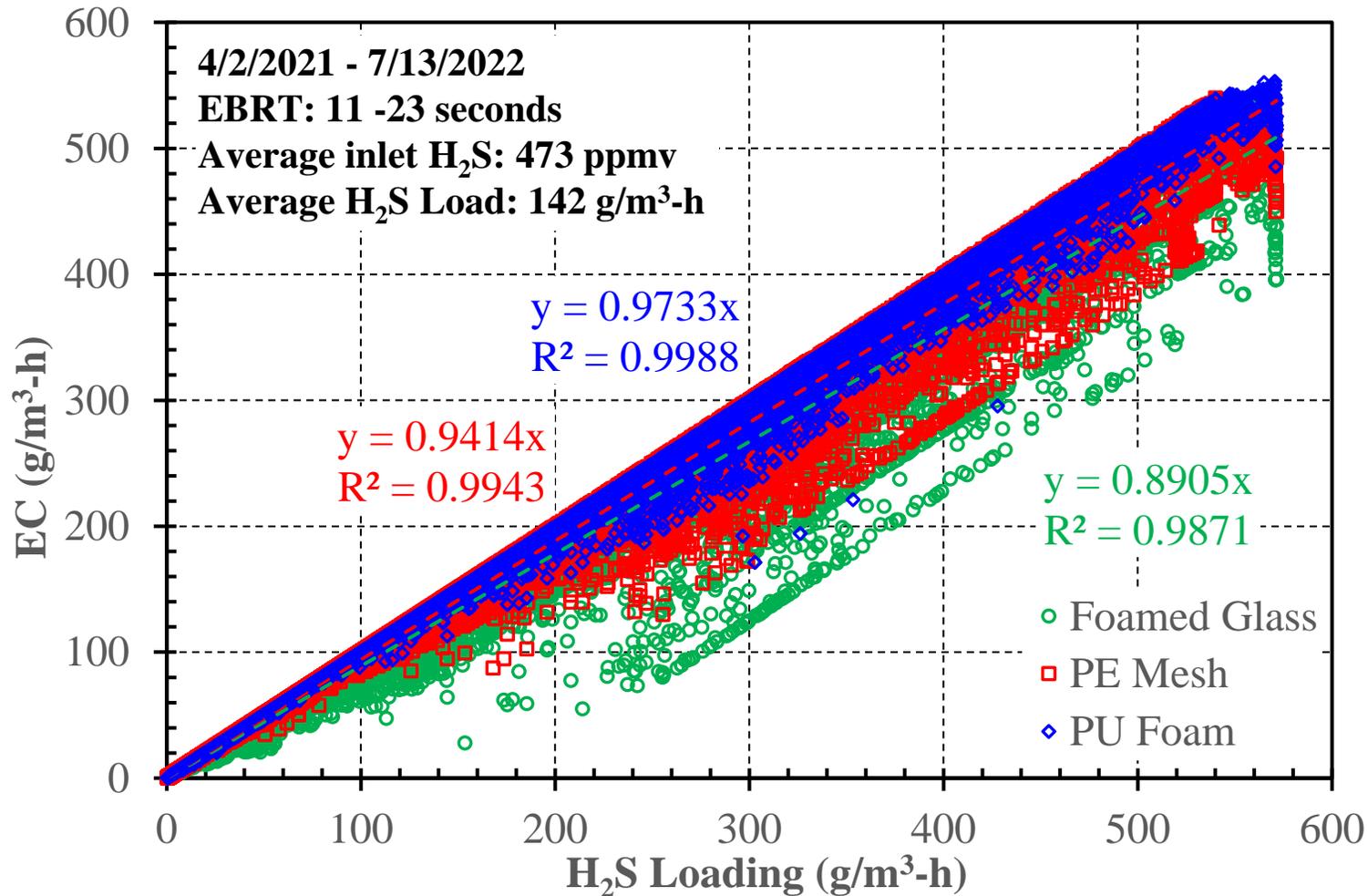
# H<sub>2</sub>S Removal vs H<sub>2</sub>S Loading



- H<sub>2</sub>S removal declines at high H<sub>2</sub>S loadings
- Foamed-glass showed the biggest drop in removal efficiency
- Can predict the BTF performance with the selected media



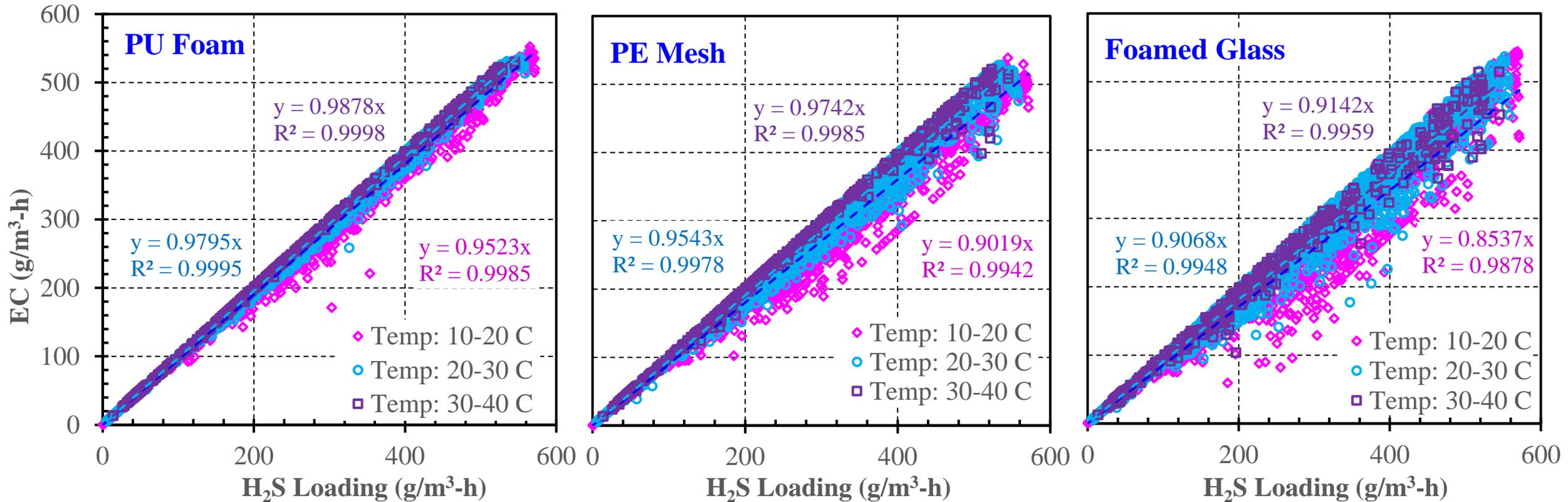
# Elimination Capacity (EC) versus H<sub>2</sub>S Loading



- PU foam provides the highest EC, followed by PE mesh, then foamed-glass
- EC increased linearly with H<sub>2</sub>S loading due to more biomass and higher removal rate



# Temperature Influence on H<sub>2</sub>S EC



- ❑ Higher and less variable EC at higher temperatures
- ❑ PU foam most consistent, then PE mesh, then foamed glass at various H<sub>2</sub>S loading and ambient temperature (diurnal and seasonal variations)



# Visual Inspection of Used Media

Media	PU Foam	PE Mesh	Foamed Glass
Top			
Middle			
Bottom			

- No signs of media compression, deformation, or deterioration
- More biofilm and elemental sulfur on the bottom



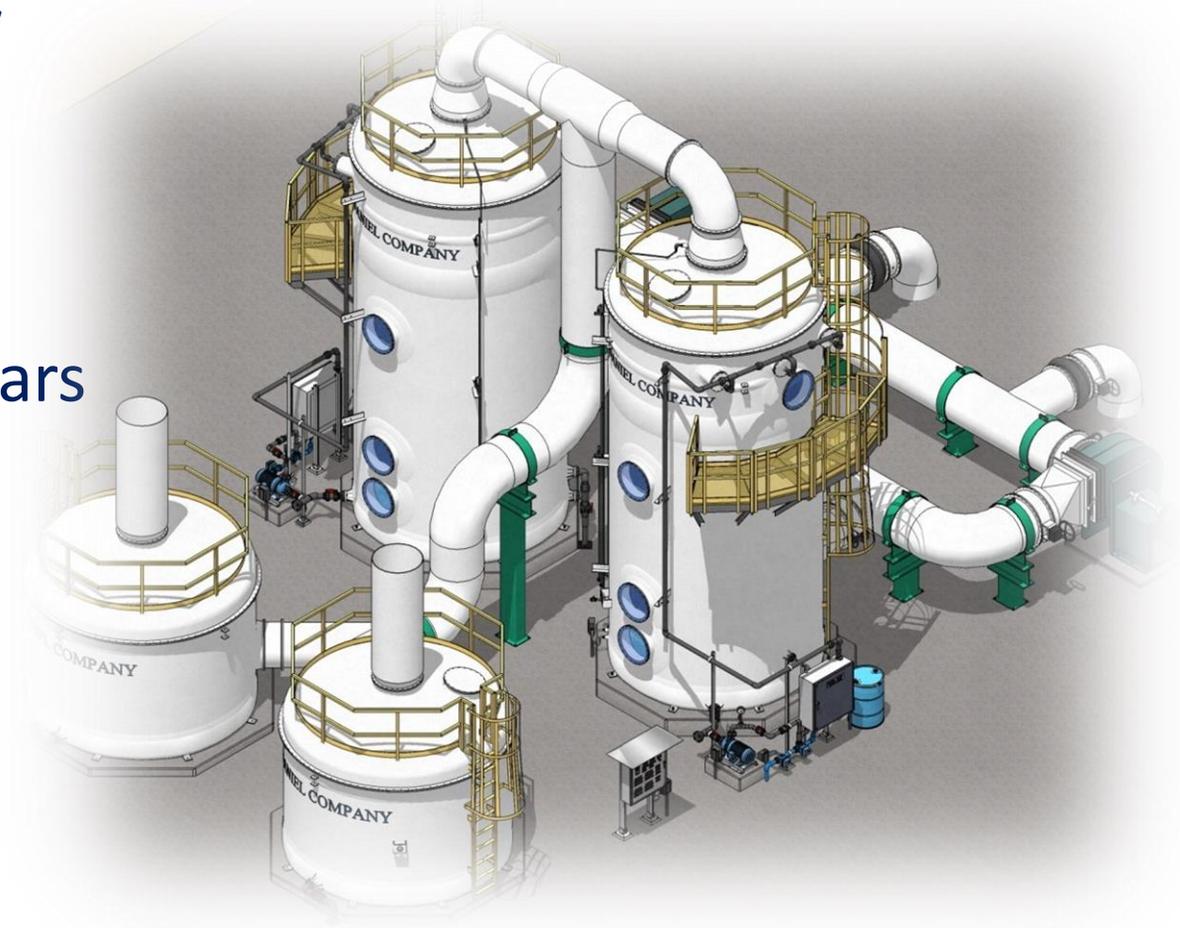
# Cost-Effective Media Selection

## ❑ Warren Facility E3 Odor Control Facility

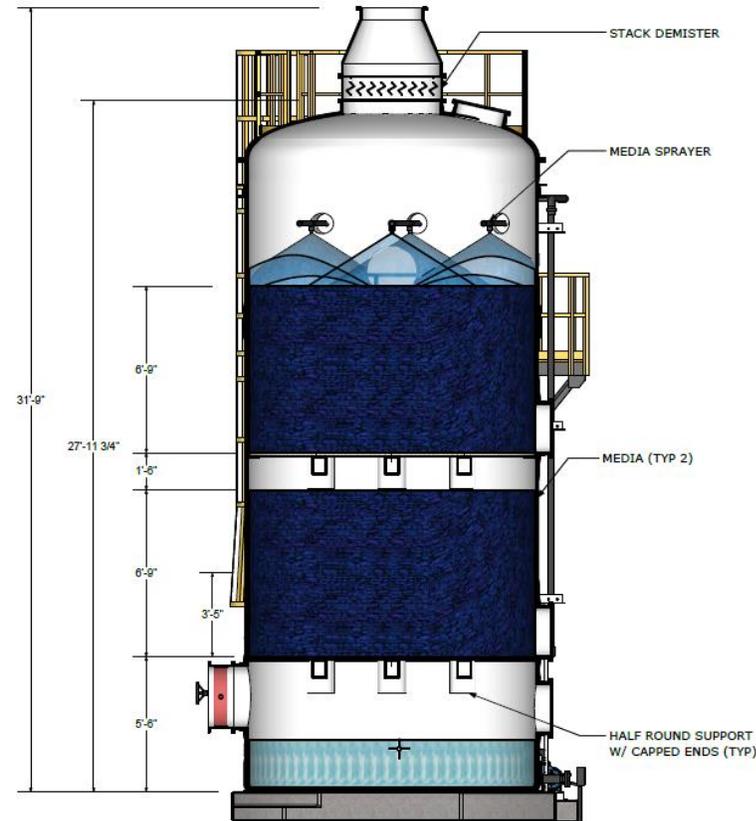
- H<sub>2</sub>S loading: ~13 g/m<sup>3</sup>-h
- Media bed depth: 12.5 ft
- Installed **foamed glass**
- Achieved > 98% removal over last 4 years
  - ✓ Inlet H<sub>2</sub>S = 50–300 ppmv
  - ✓ Outlet H<sub>2</sub>S ≤ 1 ppmv

## ❑ LCWRP Odor Control Facility

- H<sub>2</sub>S loading: ~60 g/m<sup>3</sup>-h
- Recommend **PU foam** or **PE mesh**, to enable longer carbon service life



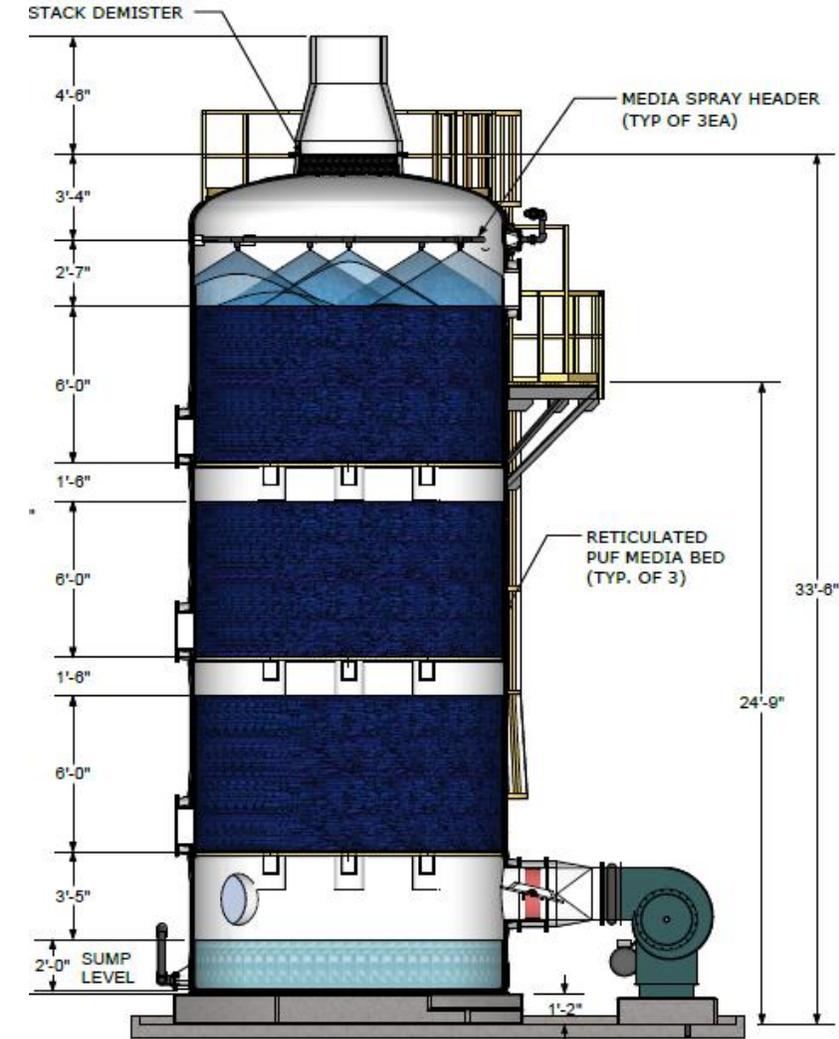
# 2 Dual-Bed BTFs vs 1 Triple-Bed BTF



	Two BTFs (Dual-Bed)	One BTF (Triple-Bed)
Footprint	2x	1x
Airflow per Vessel	1x	2x
Superficial Velocity <sup>a</sup>	1x	2x
H <sub>2</sub> S Load Per Vessel <sup>b</sup>	1x	2x

<sup>a</sup> Velocity  $\propto$  Headloss

<sup>b</sup> Load  $\propto$  Fouling potential



# Carbon Scrubbers

## ❑ Necessity

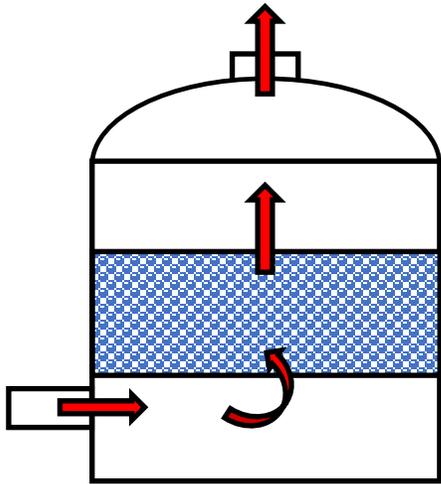
- Always meet the AQMD H<sub>2</sub>S limit of 0.5 – 1 ppmv H<sub>2</sub>S?
- Daily H<sub>2</sub>S breakthrough in BTF outlet?

## ❑ Redundancy

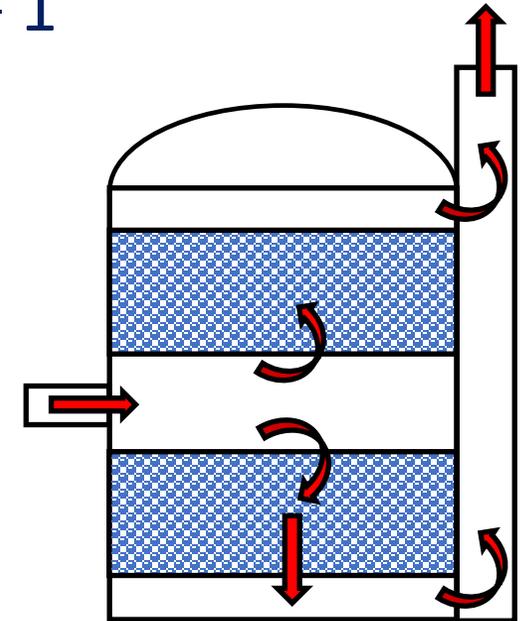
- Frequency of carbon changeout

## ❑ Single-Bed vs Dual-Bed

- Dual-bed may lower capital cost and footprint required, but it is difficult to replace carbon media in the bottom bed



Single-Bed  
Carbon Scrubber



Dual-Bed  
Carbon Scrubber



# Breakthrough Time for Activated Carbon

GAC	Unit Cost (\$/lb)	Adsorption Capacity (g-H <sub>2</sub> S/mL)	Breakthrough Time (days)
Regular Coconut Shell	\$1.95	0.03	<b>3 – 5</b>
Caustic Impregnated	\$2.62	0.3	<b>49 – 62</b>
Extruded Cylindrical Pellet	\$2.15	0.2	<b>77 – 96</b>

Notes:

- Mean particle diameter: 4 mm
- Regeneration cost: \$0.55/lb

Worth considering alternative carbons even without carbon regeneration

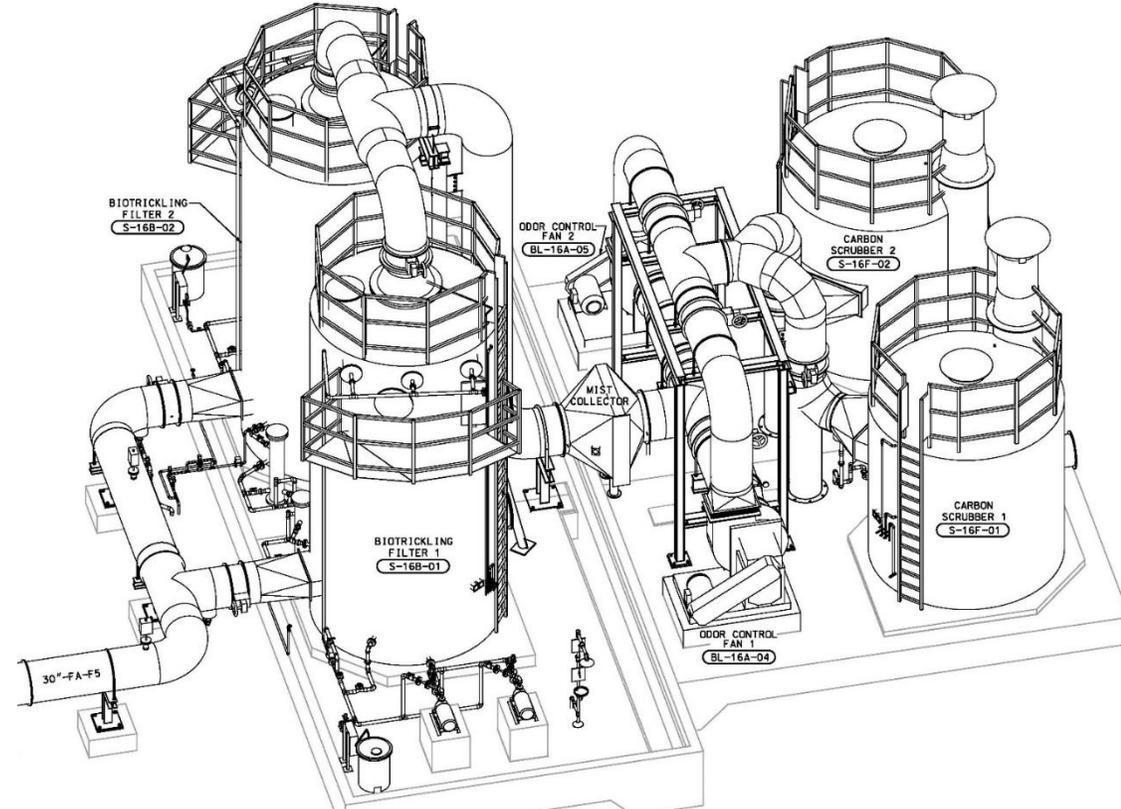


# Proposed Design

Unit	Description	Value
BTF (2 duty)	Media bed diameter (feet)	12
	Media bed depth (feet)	12.4 (Typ. <7)
	EBRT (sec)	<b>14</b>
	Superficial velocity (ft/min)	53 (Typ. 50-100)
Carbon Scrubber (2 duty)	Bed diameter (feet)	12
	Carbon bed depth (feet)	<b>3</b>
	EBRT (sec)	3.4 (Typ. >3)
	Superficial velocity (ft/min)	53 (Typ. 50-60)

## Notes:

- Design based on air flow rate of 12,000 cfm
- Maximum bed diameter for truck delivery = 12 ft



# Cost Analysis for BTF Media and Activated Carbon

BTF media	Unit	PU Foam (\$25/ft <sup>3</sup> )	PE Mesh (\$50/ft <sup>3</sup> )	Foamed Glass (\$10/ft <sup>3</sup> )
Annual Cost for BTF Media	\$/year	<b>7,000</b>	<b>14,000</b>	<b>2,800</b>
Annual Cost for BTF Media & Regular Carbon (\$1.95/lb)	\$/year	<b>14,700</b>	<b>23,900</b>	<b>83,100</b>
Annual Cost for BTF Media & Extruded Pellet Carbon (\$2.15/lb)	\$/year	<b>10,700</b>	<b>18,700</b>	<b>41,300</b>

- PU Foam and Extruded Pellet Carbon is best combination**
- Higher cost of PU foam or PE Mesh would be **offset by lower annual cost for carbon**



# Conclusions

- ❑ Under **low H<sub>2</sub>S loading**, similar performance by all three media with nearly complete removal
- ❑ Under varying **H<sub>2</sub>S loading** and **temperature** conditions, **most consistent and highest H<sub>2</sub>S removal** by PU foam, then PE mesh, then foamed glass
- ❑ Differences in performance appear related to media properties: better performance with higher **accessible specific surface area** and **porosity**
- ❑ **Selecting the appropriate BTF media** based on the **estimated H<sub>2</sub>S loading** ensures **reliable and cost-effective odor control**





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# Questions?

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OUR SERVICE AREA